

Stokes-Einstein equation to determine D and d (More common)

► For a solution of given viscosity (η), at a constant temperature (T), the rate of diffusion is given by the **Stokes-Einstein equation (Accept)**,

$$D = (kT) / (6\pi\eta d)$$

- Measure intensity (I) at various time interval (τ),
- $I(0) = I(\tau)$ for short $\tau \rightarrow$ "Correlated"
- Define **auto-correlation function**, $G(\tau) = \langle I(t) I(t+\tau) \rangle =$ Average of the intensity product. Correlation decreases as τ increases.
- High $G(\tau)$ means particles have not diffused away during τ .
- Thus $G(\tau)$ remaining high for a long time interval indicates **large, slowly** moving particles.

The time scale of fluctuation is called **decay time** which is related to the particle size. **Decay constant** (Γ) $\equiv 1/\text{Decay time}$

Large, slowly moving particles \rightarrow long decay time and small Γ

For mono-disperse sample

$$G(\tau) = A_o + Ae^{-2\Gamma\tau}$$

$$\Gamma = \text{decay constant} = DQ^2$$

$$D = \text{diffusion coefficient} = \frac{kT}{6\pi\eta d}$$

$$Q = \text{scattering vector} = \left(\frac{4\pi}{\lambda}\right) \sin\left(\frac{\theta}{2}\right)$$

A_o = Background signal, A = Instrument constant,

Procedure to determine D and d.

Measure $G(\tau)$ vs. τ

Calculate $G(\tau)$ using $G(\tau) = \lim_{T \rightarrow \infty} \left(\frac{1}{T}\right) \int_0^T I(t)I(t+\tau)dt$ (a)

Fit the data to $G(\tau) = A_o + Ae^{-2\Gamma\tau}$ and determine Γ

Determine D using $\Gamma = DQ^2$

Determine d using Stokes-Einstein equation,

3.7 Molecular weight of polymers

MW policy : High enough for good physical properties and low enough for processing, and varies with type and applications.

PVC: 60,000-90,000 g/mol

PMMA-Plexglas > 1x10⁶

Cellulose: Naturally over 10⁸ with Mw/Mn=10-50

For application as rayon, cellulose is degraded to 50,000-80,000

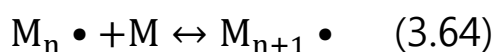
3.7.2 Thermodynamics and kinetics

3.7.2.1 Thermodynamics of chain polymerization

Gibbs energy is related to the equilibrium constant

$$\Delta G^0 = -RT \ln K \quad (3.63)$$

For chain polymerization of monomer M:



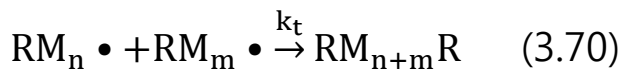
The equilibrium constant, K is defined as

$$K = \frac{k_p}{k_{ap}} = \frac{[M_{n+1} \bullet]}{[M_n \bullet][M]} = \frac{1}{[M]} \quad (3.65)$$

When the forward and backward reactions have the same rates, concept of **ceiling and floor temperature** arises (Applied for most polymers). **Ceiling temperature** is used for **recycling** whereby scraped

polymer is heated under anaerobic condition to allow distilling off the reactant molecules.

3.7.2.2 Kinetics of chain polymerization



Under steady state, $R_i=R_t$, and rate of polymerization is

$$R_p = k_p \left(\frac{k_i}{k_t} \right)^{1/2} [M][I]^{1/2} \quad (3.71)$$

Note the first order wrt $[M]$ and 1/2 order wrt $[I]$

The kinetic chain length, at steady state is

$$\nu = \frac{R_p}{R_i} = \frac{R_p}{R_t} = \frac{k_p[M]}{2(fk_i k_t [I])^{1/2}} \quad (3.72) \text{ <f=Initiator efficiency factor~0.8>}$$

The number average DP (3.72)=2 ν for coupling, which gives 1.5 PDI, while disproportionation (termination by chain transfer) yields 2.0PDI.

3.7.2.3 Thermodynamics of step polymerization

Consider a polyesterification,



The equilibrium constant is given by

$$K = \frac{[\text{COO}][\text{H}_2\text{O}]}{[\text{COOH}][\text{OH}]} \quad (3.74)$$

The fractional conversion is given by $[\text{COO}] = p[\text{M}]_0$, where $[\text{M}]_0$ is the concentration of ester group. Then

$$\text{DP}_n = \frac{1}{1-p} \quad (3.75)$$

And the corresponding weight average degree of polymerization is given by

$$\text{DP}_w = \frac{1+p}{1-p} \quad (3.76)$$

Then

$$\text{PDI} = 1 + p \quad (3.77)$$

As $p \rightarrow 1$, $\text{PDI} \rightarrow 2$ (Most probable distribution).

3.7.2.4 Kinetics of step polymerization

For self-catalyzed reaction,

$$\frac{-d[\text{COOH}]}{dt} = k[\text{COOH}]^2[\text{OH}] \quad (3.78)$$

Assuming equal molar concentrations of carboxyl and hydroxyl groups to start, the extent of reaction is given by

$$\frac{1}{(1-p)^2} = 2[M]_0kt + 1 \quad (3.79)$$

3.7.3 Molecular weight distributions

Bifunctional monomer ($f=2$, vinyl monomers) → Linear polymer)

Trifunctional monomers → Branched or cross-linked polymers

Cross-linker=Glycerol (condensation), divinyl benzene (chain rxn)

When will gelation occur?

Gelation=A single molecule extends throughout polymerization vessel

The critical extent of reaction, P_c at the gel point is

$$P_c = \frac{1}{(f-1)^{1/2}} \quad (3.83) \quad (\text{Flory and Stockmayer})$$

f =Functionality of the branch unit