1 Structure of Molecule

1.1 IntroductionPolymer = poly (many) + meros (members)Note: Macromolecule

Ex) Polyethlene φ_1 -[CH₂-CH₂]_n- φ_2 n = O(10⁴) Typically, 10³ (Wax) < MW < 10⁶ (UHMWPE) UHMWPE needs gel spinning in solvent such as decalin.

At given temperature and pressure, state of matter changes as the molecular weight increases as: $Gas \rightarrow Liquid \rightarrow Slurry \rightarrow Wax \rightarrow Solid$

 φ_{1} , φ_{2} = end group = initiator fragment = minute amount \rightarrow Exerts negligible effect on property.

Exception: POM (1N1) (Developed by Stadinger in 1920s)

 φ_1 -[CH₂-O]_n- $\varphi_2 \rightarrow$ n CH₂=O (Unzipping)

With only the development of stable end cap, POM has been commercialized in 1959 as engineering plastics as gear and appliance.

Mechanical properties of polymer = f (MW, Structure) Effect of MW Break strength = A - B/Mn A, B = Constant Mn = Number average MW





Processing method controls the MW:
Injection grade < Extrusion grade < Film grade
Injection=Flow is most important.
Film=Melt strength is most important.

► Effect of molecular structure Linear PE = easy to crystallize = high density PE(HDPE) Produced by Ziegler-Natta catalyst (low pressure method) Less than 1 branch per 100 main chain C atoms High crystallinity→high density($\rho = 0.97-0.98$ g/cm³)→ for heavy duty

Branched PE (BPE)

Short chain branch disturbs chain packing into crystal structure→low crystallinity →low density Small amount SCB exerts significant effects on solid state property - modulus, creep resistance, impact toughness. Long chain branch exerts significant effect on melt property.

Low density PE =LDPE (SCB) (High pressure method). 2-3 branches per 100 main chain C atoms.



Mostly 2 or 4 carbon atoms per branch (SCB).

Low crystallinity \rightarrow low density ($\rho = 0.92 - 0.93$).

Type of BPE LDPE by back biting mechanism (Eq VI)



LLDPE, ULDPE, VLDPE Density (0.86< ρ < 0.89) Produced by copolymerization w/ α -olefin Typically 1-butene, 4-methyl pentene-1 (Z-N catalyst) (Figure 1.4)

Type and content of α -olefin governs the property and applications. LLDPE-vinyl sack (high tear strength!!!) ULDPE, VLDPE-olefin modifier, hot melt, adhesives... Toughmer (Mitsui, commercialized in 1986) --- See Table 1 Figure 2 Series A=copolymer with butene-1, Tm=70-80°C Series B=copolymer with 4-methylpentene-1, Tm ~ 40°C



1.4 An illustration of polymerization by Ziegler-Natta catalyst. The monomers diffuse on to the catalyst surface. They then migrate across the surface to the growth point.

Sample	Density (g/cm ³)	Tm (°C)	MI (g/10min)*	Mn (10 ⁴)	Mw (10 ⁴)	Comonomer	C2 u	nits	Maker
A-4085	0.887	75.2	3.7/ 23.0	5.52	9.95	butene-1	86 %	mol	Mitsui
A-4090	0.893	82.0	3.9/ 24.0	3.75	6.99	butene-1	86 %	mol	Mitsui
A-20090	0.895	84.2	18.2/114.5	2.81	4.78	butene-1	86%	mol	Mitsui
P-0480	0.865	40.8	1.0/ 6.6	6.66	14.20	4-methylpentene	76%	wt	Mitsui
P-0680	0.867	40.0	0.4/ 3.1	8.88	17.21	4-methylpentene	76%	wt	Mitsui
E308 HDPE)	0.956	129	0.84/ 11.2	2.13	8.59	<u>.</u>	100%	wt	Korea Petrochen

Table 1. Characteristics of ULDPEs and HDPE



Crosslinked PE (X/L PE)



1.2 Illustration of the molecular structure of cross-linked polyethylene in the liquid state. The spaces between the sketched net are filled with other parts of the network.

Produced by melt extrusion in the presence of peroxide (DCP, BPO).

Properties of X/L PE

High ESCR (Environmental stress crack resistance).

High impact strength.

Used for hot water pipeline.

Peroxide cure of PP Chain session (β -scission) Called rheology controlled PP.

1.2 Additional polymers

► Vinyl monomer

$$\begin{array}{cccc} n \ CH_2 = CH & \longrightarrow & - \ (CH_2 - CH)_n - \\ & & & | \\ & X & & X \\ \end{array}$$

-H, -CH₃, -Cl, \bigcirc

PE, PP, PVC, PS (4 Commodity Polymers)

► Acrylate : Acrylic acid derivative

$$\begin{array}{cccc} n \ CH_2 - \ CH & \longrightarrow & - \ (CH_2 - \ CH)_n - \\ & & | \\ C = \ O & & C = \ O \\ & | \\ OH & & OH \end{array}$$

Methyl acrylate

Ethyl acrylate

Butyl acrylate...w/ increasing length, Tg decreases until the branch is crystallized. Methacrylic acid

MMA.....

Mechanism & Kinetics

$$n CH_2 = CH \longrightarrow -(CH_2 - CH)_n -$$

Decomposition

$$I \xrightarrow{k_d} 2R \cdot \qquad \qquad R_d = 2 f k_d [I]$$

Initiation

$$R \cdot + M \xrightarrow{k_i} M_1 \cdot \qquad \qquad R_i = R_d = 2 f k_d [I]$$

Propagation

$$M_n \cdot + M \xrightarrow{k_p} M_{n+1} \cdot \qquad R_p = k_p \left[M \cdot \right] \left[M \right] = k_p \left(\frac{f k_d \left[I \right]}{k_t} \right)^{1/2} \left[M \right]$$

Termination

$$egin{aligned} &M_n \cdot + M_m \cdot \ rac{k_{tc}}{\longrightarrow} \ M_{n+m} \cdot \ ext{(Coupling)} \ &M_n \cdot + M_n \cdot \ rac{k_{td}}{\longrightarrow} \ M_n + M_m \ ext{(Disproportionation by H transfer)} \ &R_t = \ 2k_{td} \ [M \cdot]^2 (Disproportionation) \end{aligned}$$

@s.s
$$R_t = R_i = 2k_{td} [M \cdot]^2$$

 $[M \cdot] = \left(\frac{2 f k_d [I]}{2k_{td}}\right)^{1/2}$

1.3 Condensation polymers

► Polyamide 66(Nylon 66)

$${}_{n H_{2}N(CH_{2})_{6}NH_{2}+n HOC(CH_{2})_{4}COH} \stackrel{O}{\underset{\longleftarrow}{\overset{reversible}{\longleftarrow}} \stackrel{O}{\underset{\longleftarrow}{\overset{O}{\longrightarrow}}} \stackrel{O}{\underset{NHC}{\overset{}}}$$

Polyester (PET), PBT

MW controlled by the stoichiometric imbalance as follow:

$$\overline{X_n} = \frac{1+r}{1+r-2rp} = \frac{1+r}{1-r} \quad (p=1)$$

- ► Condition for high MW by condensation polymerization
 - i) 1:1 stoichiometry
 - ii) Pure monomer

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- iii) Long reaction time
- ▶ Radical polymerization vs Condensation polymerization

► Radical polymerization : Initiation + Propagation + Termination

► For condensation polymerization high MW is obtained only at long reaction time with exact 1:1 stoichiometry



reaction time